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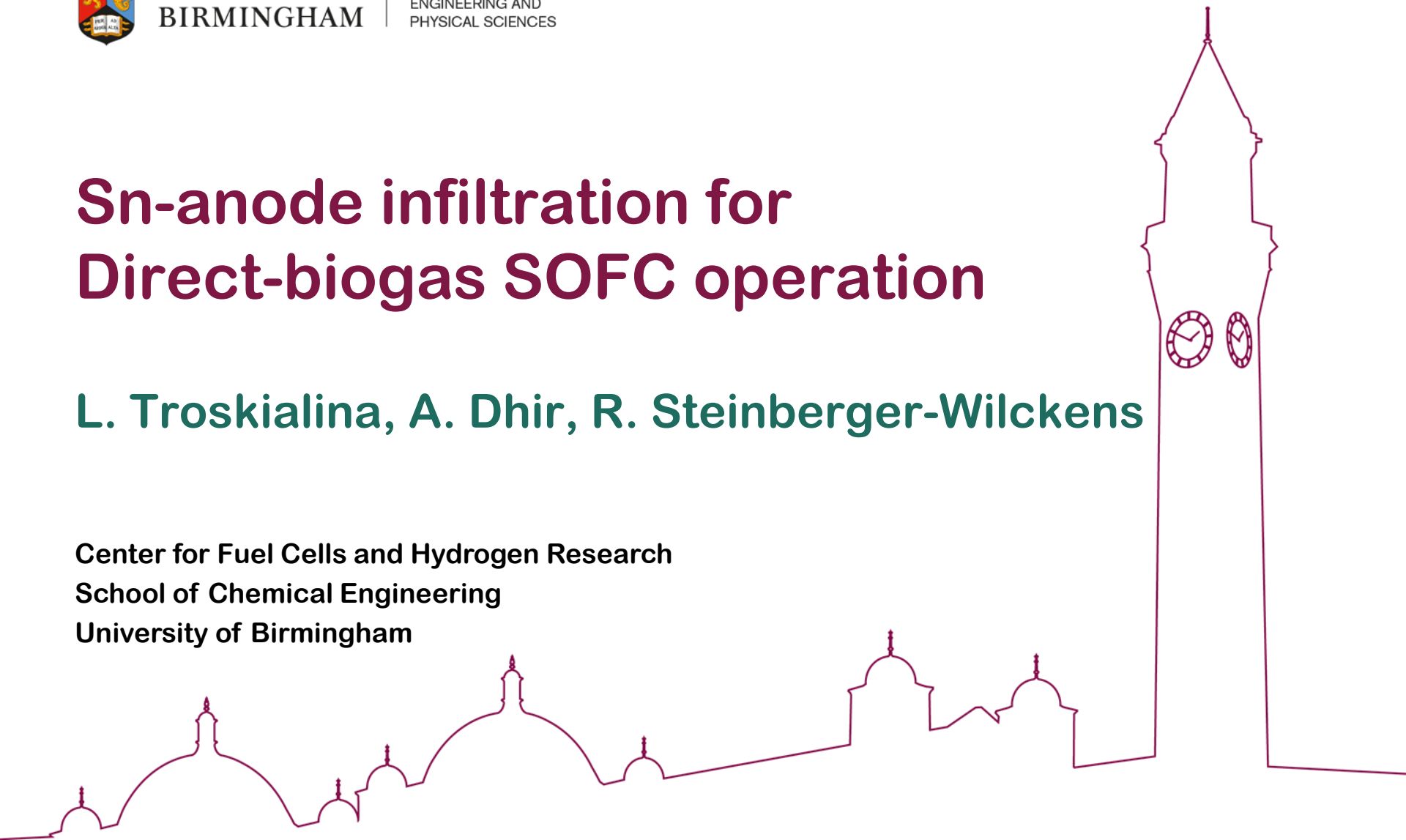
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# Sn-anode infiltration for Direct-biogas SOFC operation

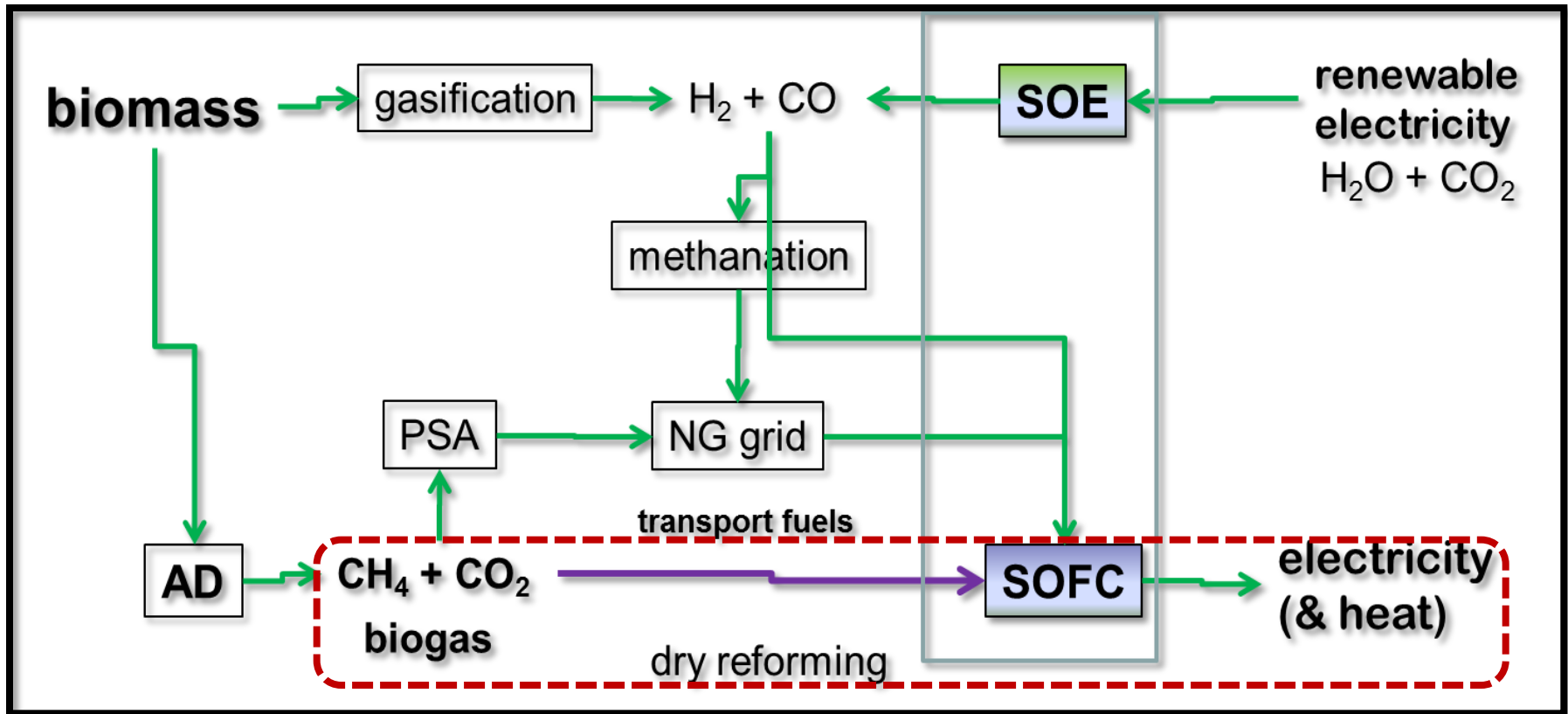
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Center for Fuel Cells and Hydrogen Research  
School of Chemical Engineering  
University of Birmingham

Fuel Cell and Hydrogen Conference, Birmingham 1<sup>st</sup> June 2017



# Aim: to contribute to sustainable direct-biogas SOFC operation

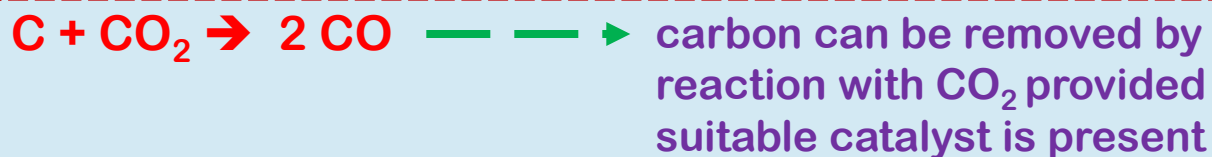


# Reactions of biogas fuel at anode

## Dry reforming of CH<sub>4</sub>



Which occurs via dissociative adsorption of CH<sub>4</sub> followed by C oxidation



- ✓ Supported Ni (on zirconia, silica, alumina, magnesia) are among the widely used catalysts for methane reforming
- ✓ Bimetallic Ni catalysts are already developed to assist in carbon removal. Ni-Sn catalyst system is one of them.

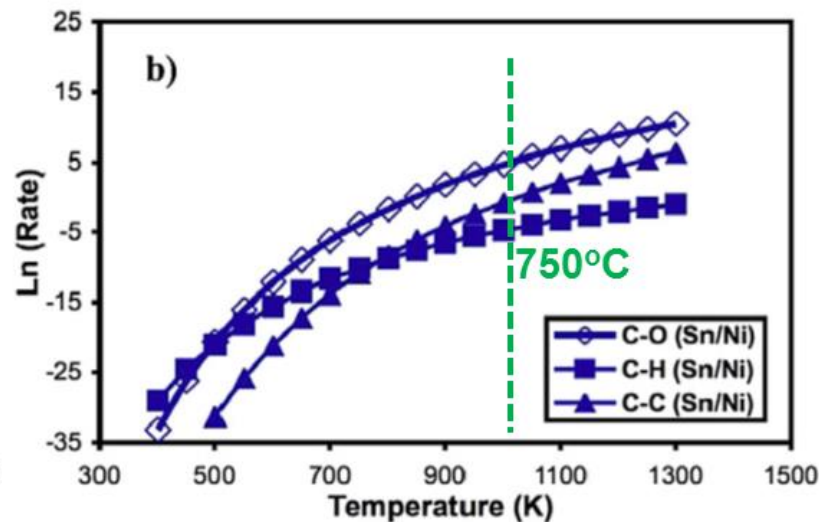
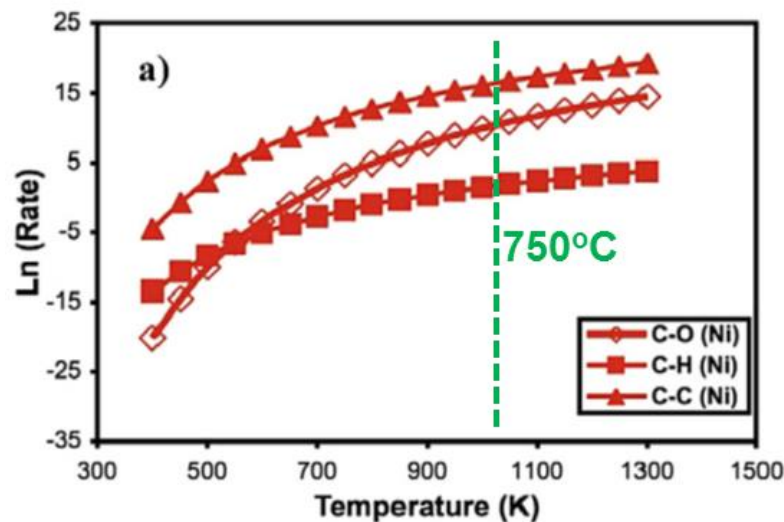
Trimm, D.L., *Catalysts for the control of coking during steam reforming*. Catalysis Today, 1999. 49(1–3): p. 3-10



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# Reference results from Calculation using Density Functional Theory (in steam reforming)



At 750°C, on both SnNiYSZ (blue) and NiYSZ (red) C-H bond activation is the rate limiting step

On NiYSZ (red) C-C bond formation is faster than C-O bond formation

On SnNiYSZ (blue) C-O bond formation is faster than C-C bond formation

Question: Will these behavior apply in dry reforming? Let's investigate!

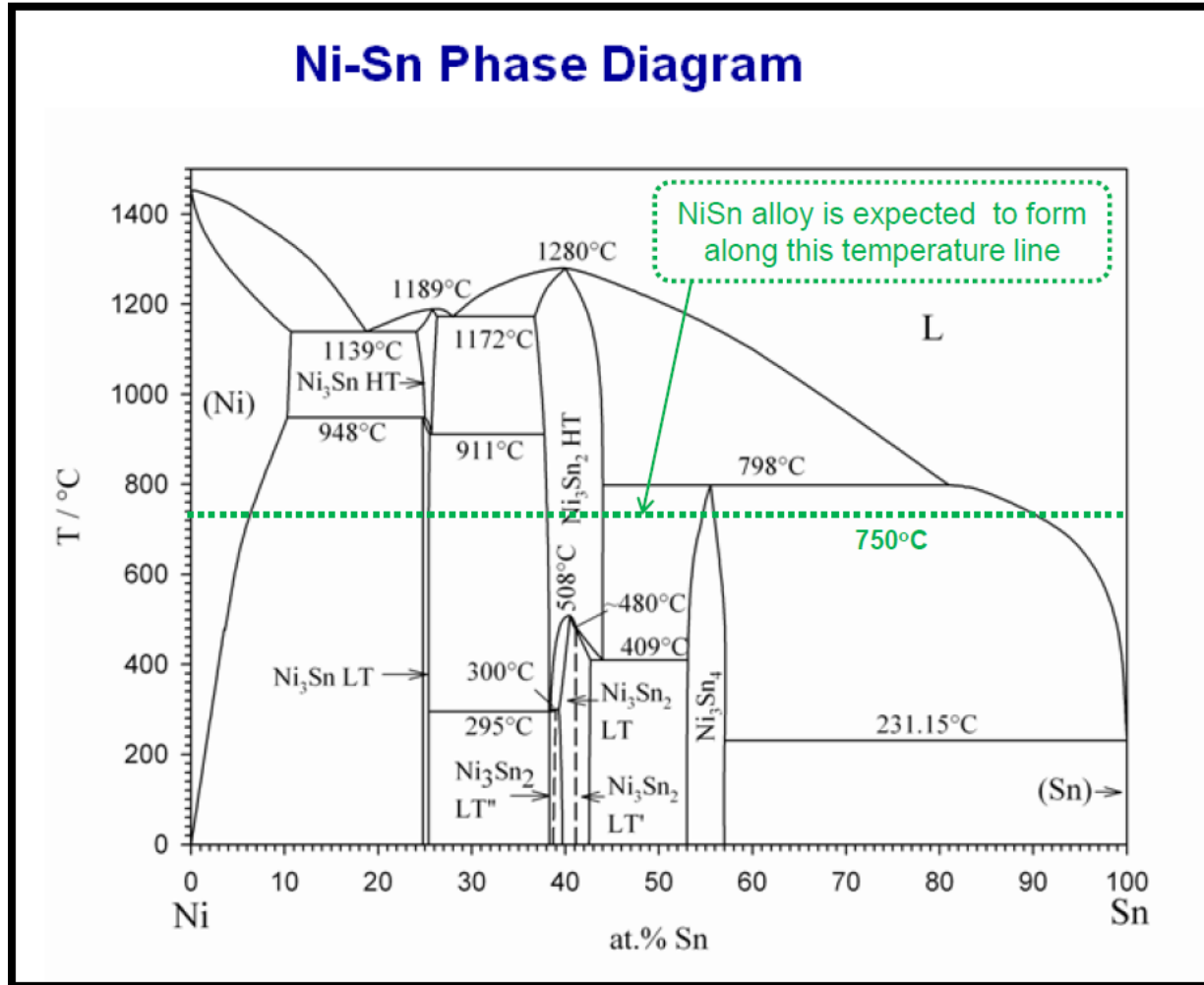


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Nikolla, E., J. Schwank, and S. Linic, *Comparative study of the kinetics of methane steam reforming on supported Ni and Sn/Ni alloy catalysts: The impact of the formation of Ni alloy on chemistry*. Journal of Catalysis, 2009. 263(2): p. 220-227

## Formation of Ni-Sn alloy at typical SOFC operating condition is expected



### Possible phases:

- ✓ Ni<sub>3</sub>Sn Low Temp.
- ✓ Ni<sub>3</sub>Sn High Temp.
- ✓ Ni<sub>3</sub>Sn<sub>2</sub> Low Temp.
- ✓ Ni<sub>3</sub>Sn<sub>2</sub> High Temp.
- ✓ Ni<sub>3</sub>Sn<sub>4</sub>

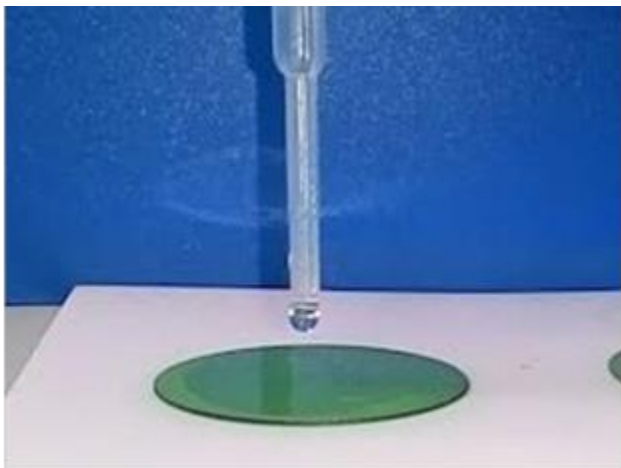
Chart adapted from Schmetterer, C., et al., *A new investigation of the system Ni-Sn*. Intermetallics, 2007. 15(7): p. 869-884



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# Sn-infiltration method



- ✓ Infiltration by pipette-drop on commercial NiYSZ anode surface
- ✓ Ø 30mm, 600mg Ni
- ✓ Multiple drops were performed

**Dopant solution:  $\text{SnCl}_2$  in ethanol**  
1 mg Sn/drop solution  
1 drop = 20  $\mu\text{l}$

## Method:

- Drop on sintered anode surface
- Air dry at ambient temperature
- Oven dry at 100-120°C
- Calcine at 600°C
- Reduce in  $\text{H}_2/\text{He}$  at 750°C
- Perform dry reforming
- **Monitor outlet gas composition using mass spectrometer**



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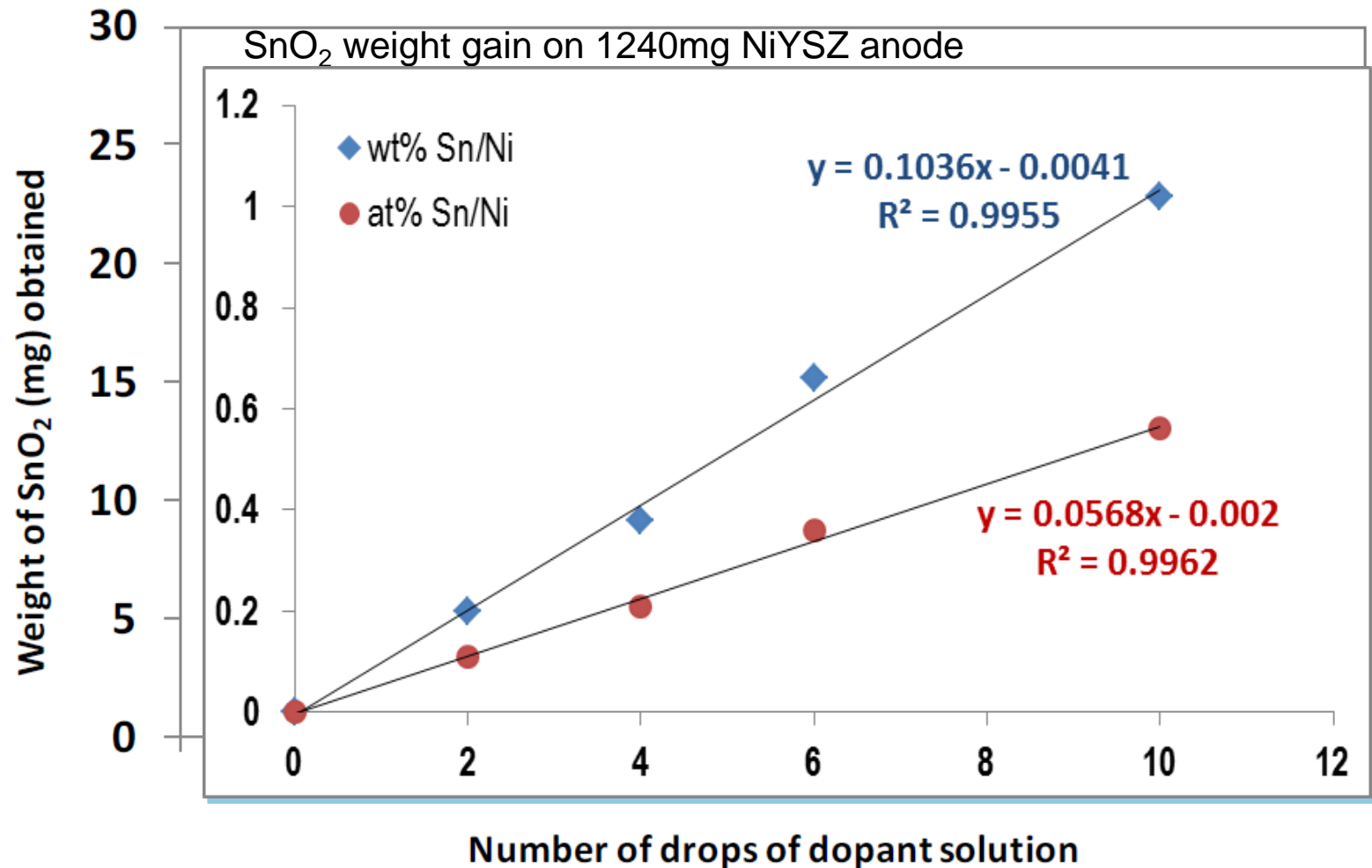
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# TGA and possible reactions of $\text{SnCl}_2 \cdot 2\text{H}_2\text{O}$ as dopant to form Ni-Sn alloys

Infiltration stage	Reactions	TG Region
Drying at 70 °C and 100 °C (Solvent evaporation)	$\text{C}_2\text{H}_5\text{OH}_{(\text{liq})} \rightarrow \text{C}_2\text{H}_5\text{OH}_{(\text{vap})}$ $\text{H}_2\text{O}_{(\text{liq})} \rightarrow \text{H}_2\text{O}_{(\text{vap})}$	1
First stage heating up to 200 °C (anhydrous $\text{SnCl}_2$ formation)	$\text{SnCl}_2 \cdot 2\text{H}_2\text{O} \rightarrow \text{SnCl}_2 + 2\text{H}_2\text{O}_{(\text{vap})}$	2
Further heating to 600 °C during calcinations ( $\text{SnCl}_2$ evaporation and calcinations)	$\text{SnCl}_2_{(\text{solid})} \rightarrow \text{SnCl}_2_{(\text{liq})}$ $\text{Partial SnCl}_2_{(\text{liq})} \rightarrow \text{SnCl}_2_{(\text{vap})}$ $\text{Partial SnCl}_2 + \frac{1}{2} \text{O}_2_{(\text{g})} \rightarrow \text{SnO} + \text{Cl}_2_{(\text{g})}$ $\text{SnO} + \frac{1}{2} \text{O}_2_{(\text{g})} \rightarrow \text{SnO}_2$	3 4
Reduction with $\text{H}_2$ at 750 °C	$\text{SnO}_2 + 2\text{H}_2_{(\text{g})} \rightarrow \text{Sn} + 2\text{H}_2\text{O}_{(\text{vap})}$ $\text{NiO} + \text{H}_2_{(\text{g})} \rightarrow \text{Ni} + \text{H}_2\text{O}_{(\text{vap})}$	
Alloy formation at 750 °C	$\text{Ni} + \text{Sn} \rightarrow \text{Ni-Sn alloys}$	



# Repeatable infiltration on sintered commercial SOFC anodes with different Sn loading

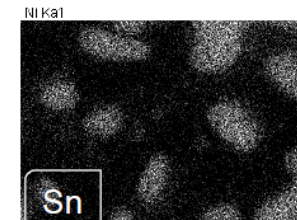
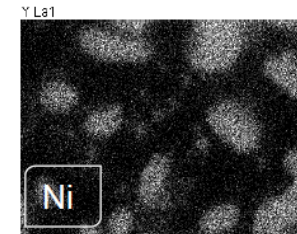
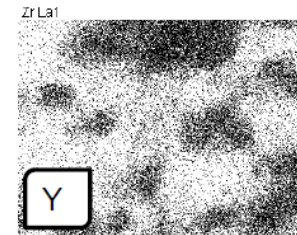
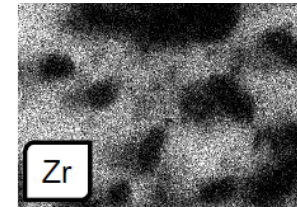
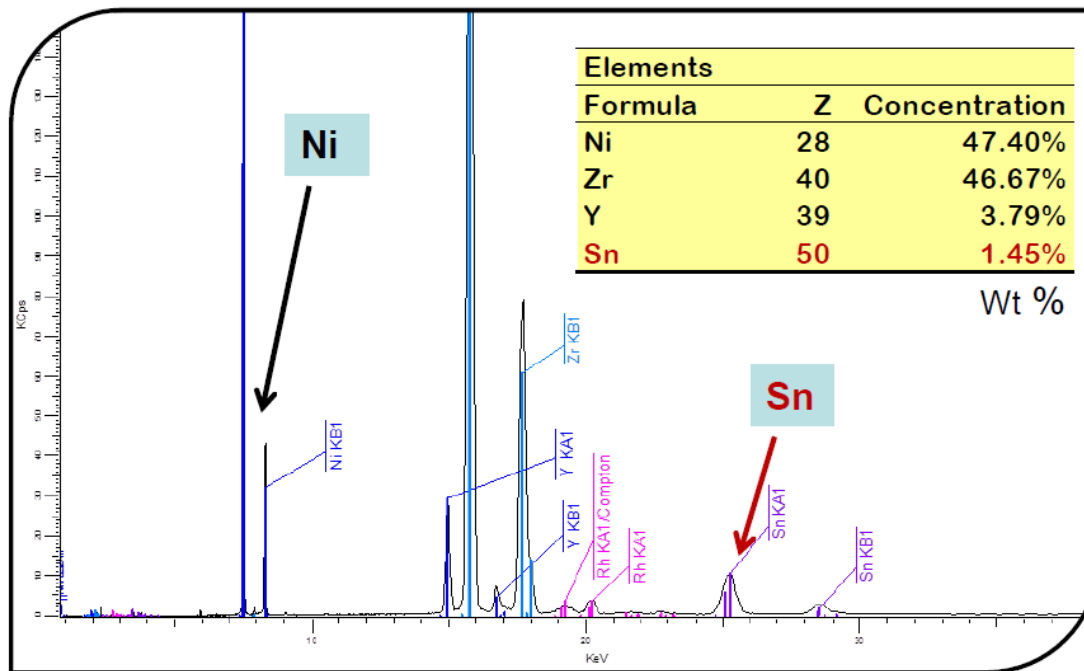




# Evidence of doped Sn

X-ray Fluorescence

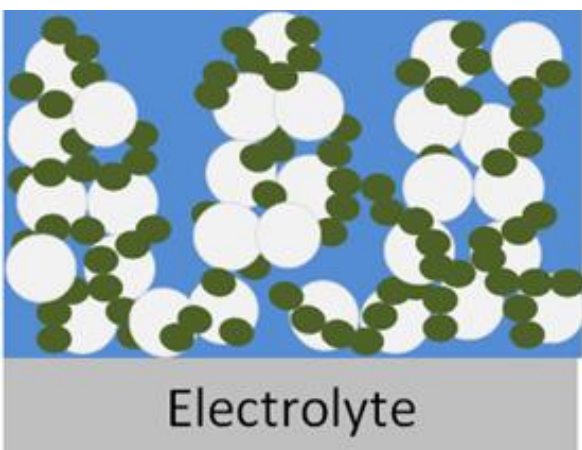
Energy-dispersive X-ray spectroscopy



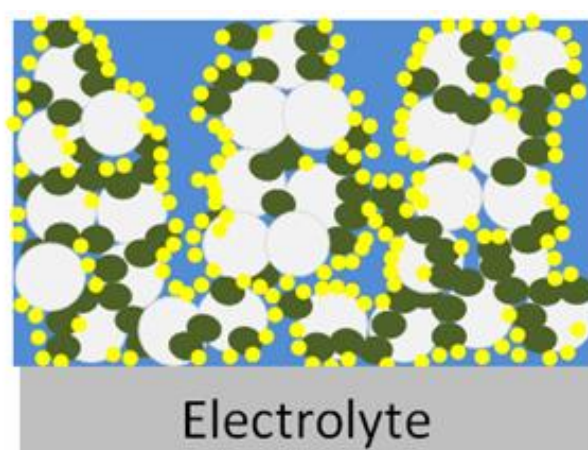
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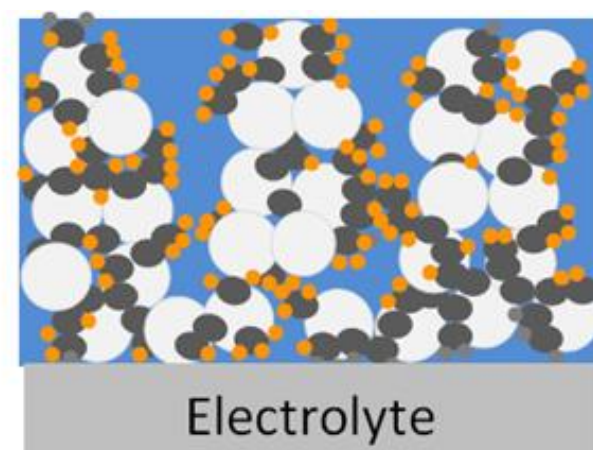
# Proposed simple structural model of Sn-infiltration using pipette-drop method on NiYSZ anode



a. Before infiltration



b. after infiltration



c. after infiltration and reduction

Legends:

○ YSZ

● NiO

● Ni

● SnO<sub>2</sub>

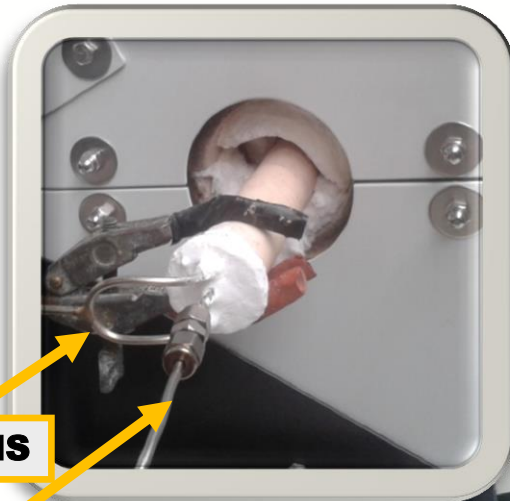
● Sn



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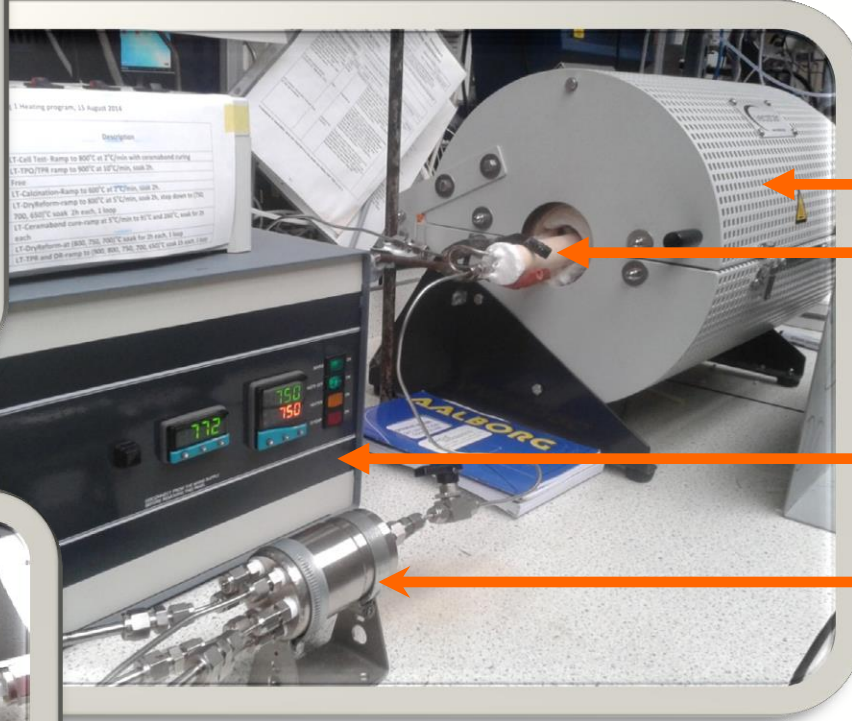
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# Dry Reforming Test Rig



**Out to MS**

**Reactants in**



**Tunnel  
Furnace**

**Quartz Tube  
Reactor/SOFC  
holder**

**Furnace  
Temp.  
Controller**

**Fuel Mixer**

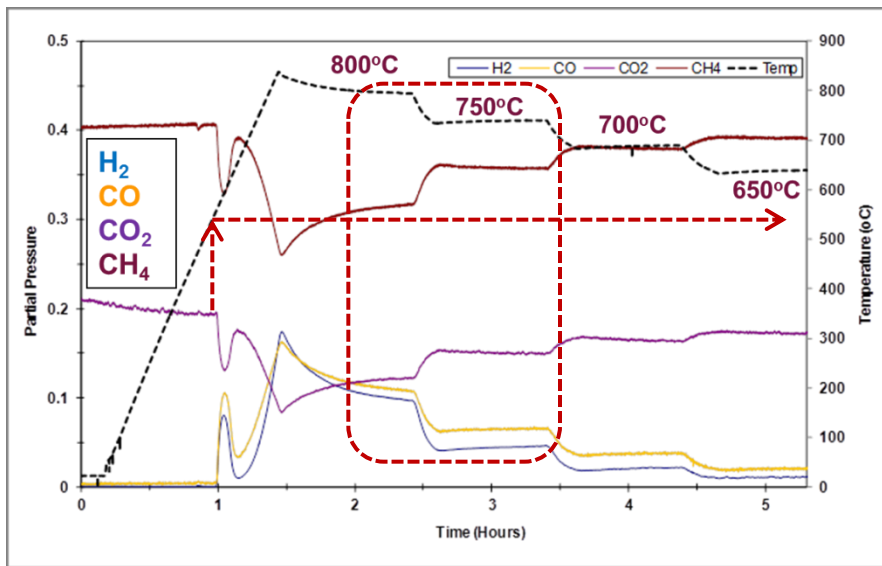


**Mass Flow  
Controllers**

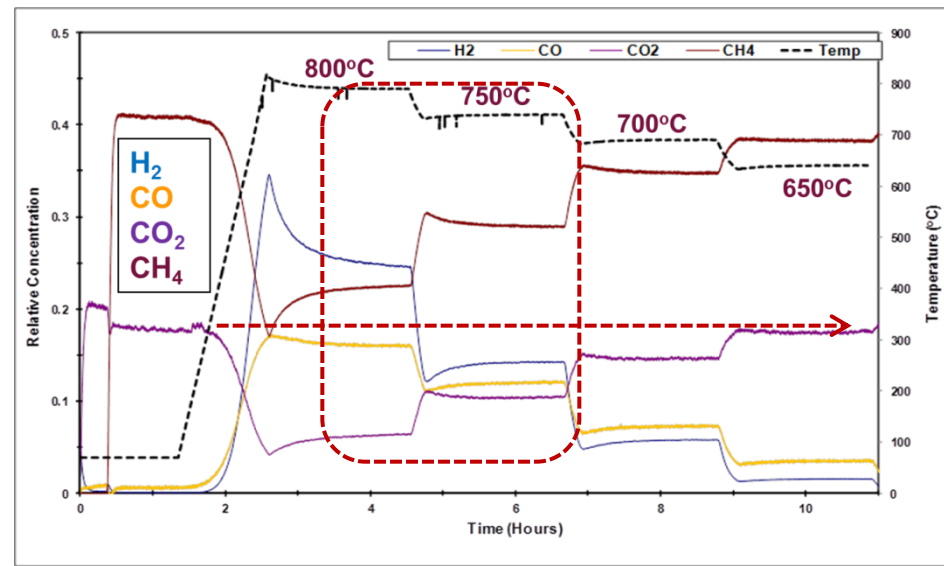
- ✓ Operating at 650 - 800°C
- ✓ Simulated biogas of CO<sub>2</sub> and CH<sub>4</sub> mixture

# Dry reforming product gas composition at varied temperature

A. on non-infiltrated SOFC anode chips



B. on Sn-infiltrated SOFC anode chips



- ✓ **Sn-infiltrated anode chips**
  - ✓ started to produce  $H_2$  and CO at 330°C while non-infiltrated ones at 550°C
  - ✓ produced much more  $H_2$  and CO than non-infiltrated ones.
- ✓ **Catalyst-activity-wise: operating SOFCs at 750-800°C in DR mode is feasible.**

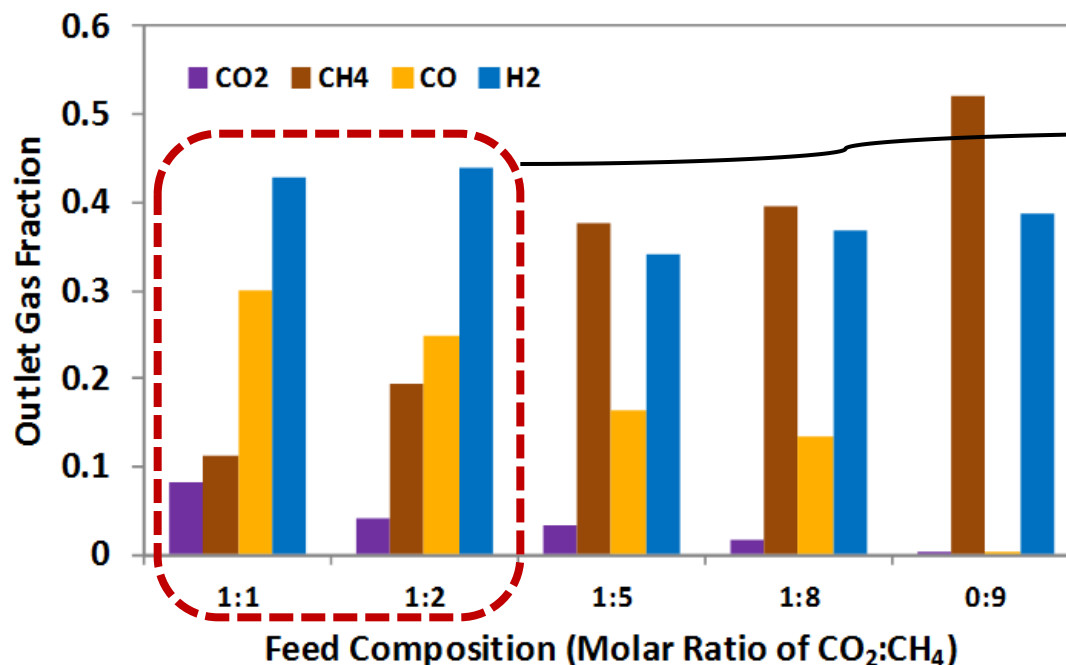


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# Product gas composition of DR on 4D Sn-infiltrated SOFC chips at different $\text{CO}_2 : \text{CH}_4$ ratio, at $800^\circ\text{C}$



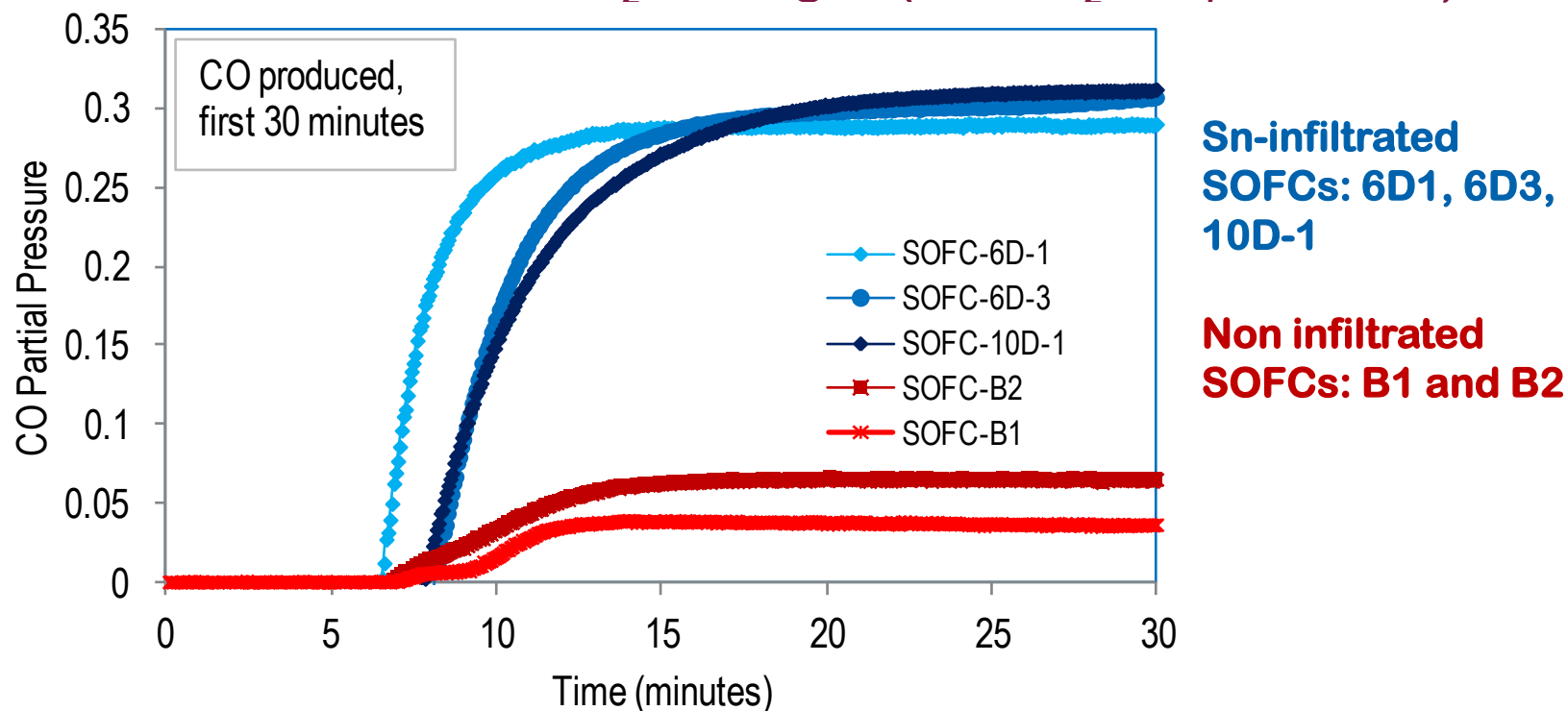
Common  $\text{CO}_2:\text{CH}_4$  compositions in biogas produced relatively high quantities of CO and  $\text{H}_2$ . These compositions will be used for SOFC operation

The bar chart is derived from Mass Spectra that records only gaseous components; so solid carbon as one of the reforming products is not shown above.

As low as 1:8  $\text{CO}_2:\text{CH}_4$  ratio produces significant amount of  $\text{H}_2$  and CO. Highest reactants conversions and amount of CO was obtained at 1:1  $\text{CO}_2:\text{CH}_4$ . Reforming at 1:2  $\text{CO}_2:\text{CH}_4$  produced similar quantity of CO and  $\text{H}_2$  to that at 1:1 ratio



# Mass spectra of SOFC outlet gas collected from 6 SOFCs at OCV when fuel is switched from H<sub>2</sub> to biogas (1:2 CO<sub>2</sub>:CH<sub>4</sub> at 750°C)



- ✓ CO level appears much higher on Sn-infiltrated SOFCs than on non-infiltrated SOFCs.
- ✓ The slope of the curves show that formation of C-O bond is faster on Sn-Ni catalysts than that on Ni catalysts which promise less carbon formation is expected on Sn-Ni/YSZ SOFCs compared to that on NiYSZ SOFCs. Further investigations are still needed.



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# Conclusions

- ❑ Sn- anode infiltration was successfully carried out on sintered anode surface, using commercially available NiYSZ anodes,
- ❑ Sn/Ni alloy presence on NiYSZ have significantly increased CH<sub>4</sub> conversion in biogas dry reforming. This finding forms a firm ground for operating SOFC directly on biogas with high power output
- ❑ Further work is on going to further
  - characterise the catalysts,
  - elucidate mechanism of biogas dry reforming,
  - elaborate on how Sn improves NiYSZ catalytic activity in DR
  - evaluate carbon formation and
  - evaluate Sn-doping on in-house SOFC anodes



# Acknowledgements

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  - ✓ Prof. Kevin Kendall and the late Dr. Waldemar Bujalski
  - ✓ Prof. Hugh Evans
  - ✓ Dr. Mark Cassidy and Prof. Tim Button
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# Thank you for your attention

## Any Questions?

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